# Trace-Metal Scavenging from Biomass Syngas with Novel High-Temperature Sorbents

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- Slip through PCDs can damage turbines, and heavy metals can escape to the environment, for IGCC systems and for chemicals and fuels production.
- Feedstock for chemical products are easier to process when stripped of alkaline and toxic metals, prior to processing.
- High-Temperature Sorbents have been shown to effectively react with and capture these metals in vitiated air and in flue gas.
- Eutectics form when sorbents react with metal.
- These sorbents have yet to be tested in reducing environments.
- In addition to the ability to capture metals, sorbents must be shown NOT to create a melted or sticky gue that will clog or damage the barrier filters.



## Pathways and Milestones – C-level and Project Milestones

biomass program

**Perennial Grasses** 

<u>Ag Residues</u> <u>Woody Crops</u>

**Pulp and Paper** 

**Forest Products** 

**Validate Cost-effective Gas Cleanup Performance** 

Validate integrated gasification and gas cleanup at pilot scale

Project Milestones	Туре	Performance Expectations			
MDP1 Move on to next phase?	D	Transport Gasifier >70% Removal of Trace Metals, without damaging or plugging the barrier filter.	Jan 2006		
MDP2 Move on to Demonstration?	D	Fluidized Bed >70% Removal of Trace Metals, without damaging or plugging the barrier filter.	Oct 2006		
Project Completion	D	Successfully Demonstrate this Technology at full-scale at the Power System Development Facility (PSDF).	Dec 2007		



## Technical Feasibility and Risks

- Sorbents have been shown to effectively and quickly scavenge Na, Pb, Cd, and other metals from vitiated air at high temperatures.
- Sorbents have not yet been tested in reducing environments.
- Sorbents will potentially melt at high temperatures, due to eutectic formation with the captured metals.
- Project subject to test schedules in larger units that are not driven by this project (i.e., PSDF).

## Competitive Advantage

- Success will eliminate corrosion issues of gas turbines and make chemical feedstocks from biomass more attractive.
- Events -- Yielding Obsolescence
  - Lack of regulation of Heavy-Metal emissions from IGCC and related systems combined with economic and durable turbine-blade coatings.
  - Indirect-fired cycles that don't need hot-gas cleanup.
  - Effective and more economical cold-gas cleanup for chemical feedstock production.

## **Project Overview**

#### biomass program

 Project Objective: Develop High-Temperature Sorbent-Injection Strategies that will effectively remove toxic and nuisance metals from syngas without damaging or plugging the barrier filter.

## U.S. Department of Energy Golden Field Office

Dr. John Scahill, Project Manager

#### Southern Research Institute

Overall Project Management
Direct and Conduct Experimental Program
Direct Modeling Effort

#### UAB

Graduate Research Assistants Graphite Furnace-AA Analysis Modeling/Testing

## Southern Company PSDF Staff

Assist with Experimental Plan and Full-Scale Demonstration

#### Gas Technology Institute

Operate High-Temperature Slipstream at RENUGAS Gasifier



## History and Accomplishments

- New Project
- Accomplishments
  - Obtained site-access agreement at PSDF.
  - Designed reaction chamber and sorbent and char feeders for slipstream tests at PSDF.
  - The syngas cleanup model development continues, building upon the present Naspeciation model.
    - Current Efforts include: adding K-speciation and heterogeneous mechanisms to the model.
    - Including sorbent/metal interactions.

## Plan/Schedule

Task and Subtask ID	Quarter #	1	2	3	4	5	6	7	8	9	10	11	12
1.0 Slipstream at PSDF	+				<b>&gt;</b>								
1.1 Sorbent screening at PSDF				<b></b>									
1.2 Parametric investigation at PSDF					<b>→</b>								
2.0 Slipstream testing or	n GTI facility												
2.1 Sorbent screening a	t GTI						<b></b>						
2.2 Parametric investiga	tion at GTI								<b></b>				
3.0 Demonstration									•			ightharpoonup	
3.1 Design, build, and install											<b></b>		
3.2 Demonstrate optimized techn.											•	-	
3.3 Sampling and Analysis											•	$\rightarrow$	
4.0 Model advancement	•												
4.1 Contributions from slipstream									<b></b>				
4.2 Contributions from full-scale													<b></b>
5.0 Low -temp and lab ea	xperiments												
6.0 Graphite furnace-AA analysis												-	
7.0 Reporting													<b></b>
MILESTONE Decision Point	s (MDP)		MDP1		<b>→</b>		MDP2		<b>&gt;</b>				



## Critical Issues and Show-stoppers

biomass program

## Critical Performance Parameters:

- How does a syngas (i.e. reducing) environment affect sorbent/metal reaction mechanisms?
- Can metal be captured without plugging or damaging the barrier filters?
- How does temperature affect capture and melting?

## Show Stoppers:

- No capture in reducing environment.
- Ineffective capture without severe melting.



## Plans and Resources for Next Stage

- If the early project stages are successful:
  - Full-scale PSDF demonstration in the third year.
- If the technology is shown to be effective and economic by the end of the project:
  - May become a standard technology that is used and further developed during all PSDF test runs.
  - Possible Full-Scale Demonstration in the RENUGAS gasifier.
  - Possible Demonstration at the 250 MW Gasifier to be built in Orlando Florida.
- Commercialization Partners:
  - Southern Company
  - Gas Technology Institute

- Southern Research Institute has recently begun this project to develop high-temperature sorbents for scavenging trace metals from syngas, without damaging the barrier filter.
- We are preparing for slipstream tests at the PSDF this summer. Modeling efforts are going forward.
- We plan to complete our current efforts early next year, followed by additional slipstream testing in the RENUGAS gasifier at GTI.
- Demonstration of this technology is planed for 2007 in the full PSDF unit, if the initial stages of the project indicate a high probability of success.

- Total Project Funding = \$962,882.00
  - -DOE = \$769,378.00
  - Cost Share = \$193,504.00
- Fiscal Year 2005 = \$323,756.00
  - -DOE = \$259,005.00
  - Cost Share = \$64,751.00